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## Lecture notes on

## Kinetics of Polymerisation

for 6<sup>th</sup> Semester students (DSE-4T)

by

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Dr. Shbhra Mishra Process of Polymerisation; Polymerisation is possible only if will defend only whom the initial and final states, not the haluse tof the linkermediate (free radical, anion, cation etc) High polymer is formed immediately in a chain reaction. Increasing shows control time simply increased the amount of high bolymes broduced. the process of Combination of the constituent morrowers is ways - a different salion and it can occur through three ways - (1) addition polymerication La condensation | polymerisation theceeres they can occur through freezadical and ionic (cationic & animid) mechanism. Asmost all enbetithents allow

lead to anionic mechanism. Electron withdrawing constituents lead to cationic mechanism. Polymerization kinelies tell us how fast the eyetem takes various reaction paths.

Addition polymerication: It can undergo through both

free radical rocanic mechanism.

() Free radical mechanism - It occurs in three steps initiation, probagation and termination. To initiate the process, come free radical producers are to be added. The organic peroxides are the common free radical producers. Azobis cisobntylonitrile (AIBN) is also a free radical producer.

HC-[-N=N-[-U] SCOD 2 Ut3-E. +N, (Initiator) T Kdyz R

(NTBN) Ut3 8ds. 2 Ut3 E. +N, (Initiator) T Kdyz R

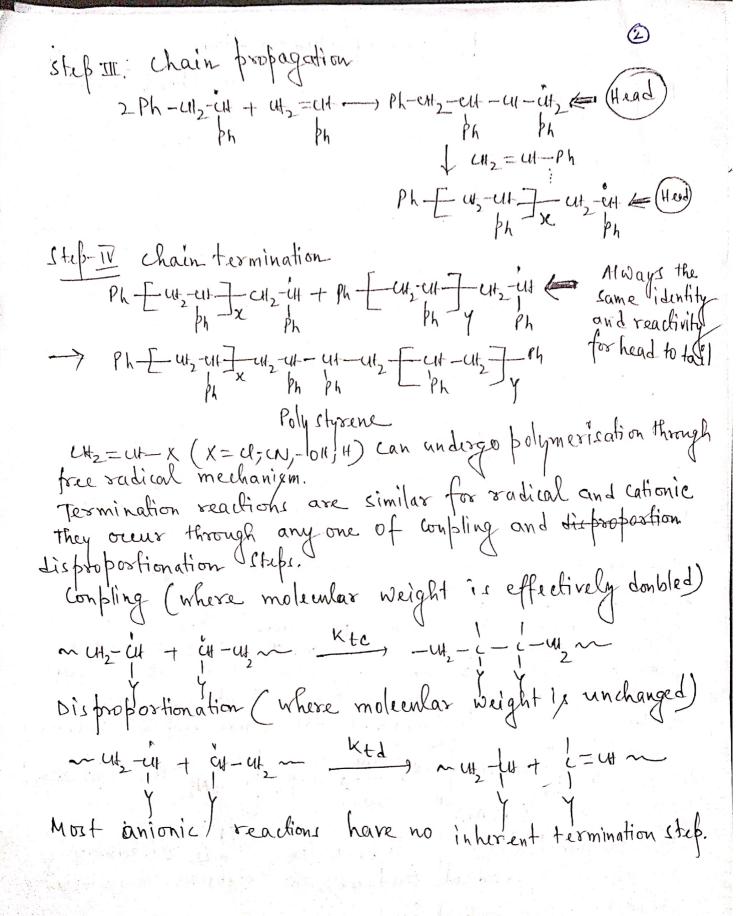
For polymerisation of styrene in presume of bunroys peroxide (tree radical producer), the steps are given below-

Step 1 6 Free radical production):0

Ph-1-0-1-1 [2Ph-1-0] -> 2Ph + 20021

Step II: chain initiation

2 Ph + 112 = cH Ph - Ph - CH2 - cH2 end)



Kirclico of fore Radical Spolymentiations Rate of reaction of polymesization is propostional to the concentration of felt or disappearance of monomer in a particular reaction. Rate of reaction = Constant x [ Concentration] terme. Rate of disappearance of monomer = - dM = K [concentration] terms for the conversion of a monomer to a polymer via free radical initiation may be described using sleady state Kinetics approaches - () (1) à Initiation: This is a of two step process involving A. decomposition of the initiator into primary radicals. I Kd. 2 R; Kd = Constant for juited or decomposition B. The addition of a monomer to the primary free R+M Ka > RM°; where, kay the rate monomer addition. radical Initiator decomposition is much slower than monomer addition, the first step of the initiation step (RA)

( Ka >> Ka) is the rate limiting step. some of the initiator

radicals may be undergo side readiens (secondary) ench as combination with another radical etc. Therefore only a fraction, of (an efficiency factor), of the initial initial only a fraction, either initials molecule produced a pair of free radicals, either one or both of which can initiate polymerication. Co, the rate expression for initiation may be written a1 - 0 ede A'T R: -d[I] ett d[M] = Kd[I]

As only a fraction of vadical initiate chain growth

TR. LJ D. draw? therefore, Ri = dEM] = 2fkd[I]

(iv) Propagation: The Successive addition of monomers during propagation may be represented as follows RM; IM Kpm RM2 RMS +M KP RM3 Ingeneral, RMX +M RP RMZII In this case, it is accumed that radical reactivity is independent at of chain length, which means all propagation steps have the same rate Constants kp. Propagation lis a fact process. 29. under typical condition, a polymer of molecular wt of about 10 may be produced in 0:15. It may therefore be accumed that number of molecule with the consumed in the propagation step is insignificant compared with the consumed in the propagation step. Thus the rate of consumpation of polymerication equal escientially the rate of consumpation at for monomer l'in the propagation etch. Thesefore, the rate to polymerication can be expressed as -RP = - dEM) = KP [M] [M] the concentrations of all chain radicals Oftype RMX. (ii) Termination: Ehain growth may be terminated at any point during polymerisation by using following one or two, me chanistid pathways · combination (compling) Mx +My Kte - Mx+y ) When Kte = rate Constant for tesmination prouse ( combination) Mx + My KEd + Mx + My where ktd, · Dispropostionation: If above both steps are kinefically equivalent, then termination may be represented as -Mx & My \_ kt p; where kt ix the vale lonstant for overall termination reaction.

50, the termination rate may be given as - $R_{t} = -\frac{d [M']}{dt} = 2 k_{t} [M']^{2}$ The factor of 2 arises from the fact that at each incidence of termination reaction, two radical disappear. remains constant which means that radicals are being produced and destroyed at equal rates (ie, Ri = Rt).  $[M'] = \left(\frac{fkd}{kt}\right)^{1/2} [T]^{1/2}$ With termination of sale appropriation of initiation Since the polymerisation rate is essentially the rate of monomer consumption during propagation, substitution the the previous expression in the rate egun of propagation, the final equation may be like autording to  $Rp = Kp \left(\frac{f k d}{k t}\right)^{\frac{1}{2}} \left[I\right]^{\frac{1}{2}} \left[M\right]$ The radical polymerisation is first order in monomer free radical polymerisation is first order in monomer concentration. This assumes that the initiator as efficiency is independent of monomer concurtation and half order in finitiator concentration. Sometimes Kinetic stray indicates that a dierease in f with dilution, although the decrease have been invariably small. Problem 1: The following the are data for the polymerication of styrene in benzene of boc with burzoyl pertoxide of styrene initiator.

[M] = 3.34 × 103 mol/m³, [T] = 4.0 mol/m³. the initial rate of polymerication.

Solution. solution: Assuming the initiator efficiency f=1, then rate of Polymerination,  $P_p = kp (kd/kt)^{1/2} [7]^{1/2} [M]$ Rp = kd (kp /kt) [] [M] [

 $= \left(3.2 \times 10^{-6} \frac{\text{m}^3}{\text{mol.}}\right) \left(0.95 \times 10^{-6} \frac{\text{m}^3}{\text{mol.}}\right) \left[4.0 \frac{\text{mel}}{\text{m}^3} \left(3.34 \times 10^{-8} \frac{\text{mol}}{\text{m}^3}\right)\right]$ Rp = 11.65 × 10 3 mol/m3-s. RP = 0.012 mol/m3\_1. Kinetic chain length: the Kinetic chain length, 2, is defined as the average number of monomers consumed by & each primary radical. So, the magnitude of the kinetic length will depend on the rate of the propagation relative to the termination rate is. (ince at Steady state the rate of initialion equals the rate of d termination, so, Pulting the value of  $\frac{RP}{Rt} = \frac{RP}{Ri}$  from the earlier equation -  $V = \frac{KP}{2(fk_1k_1)^2} \cdot \frac{[M]}{[I]^2}$